## **Euler's Equation for Inviscid Fluid Flow**

 Euler's equation for *inviscid* (*i*.*e*. *dissipationless*) fluid flow is a special/limiting case of the more general {non-linear} Navier-Stokes equation – which expresses Newton's 2<sup>nd</sup> law of motion for  ${compossible}$  fluid flow. The N-S eq'n, in the absence of external driving forces is:

$$
\tilde{\rho}\left(\vec{r},t\right) \frac{D\vec{\tilde{u}}\left(\vec{r},t\right)}{Dt} = -\vec{\nabla}\tilde{p}\left(\vec{r},t\right) + \left(\frac{4}{3}\eta + \eta_{B}\right)\vec{\nabla}\left(\vec{\nabla}\cdot\vec{\tilde{u}}\left(\vec{r},t\right)\right) - \eta\left(\vec{\nabla}\times\left(\vec{\nabla}\times\vec{\tilde{u}}\left(\vec{r},t\right)\right)\right)
$$

 The two *dissipative* terms on the right-hand side of the Navier-Stokes equation – a non-zero gradient of the divergence of the particle velocity  $\vec{\nabla}(\vec{\nabla}\cdot\vec{\tilde{u}}(\vec{r},t))$  and the curl of the *vorticity* of the particle velocity  $\vec{\nabla} \times (\vec{\nabla} \times \vec{\tilde{u}}(\vec{r},t))$  are associated with the *coefficient* of shear viscosity of the fluid  $\eta$ , and the *coefficient of bulk viscosity* of the fluid  $\eta_B$ , both of which have SI units of Pascal-seconds (*Pa*-*s*).

The time derivative term on the left-hand side of the Navier-Stokes equation,  $\frac{D\tilde{u}(\vec{r},t)}{T}$ *Dt*  $\frac{\vec{a}(\vec{r},t)}{2}$  is the complex particle *acceleration* associated with an infinitesimal volume element *V* of fluid  ${e.g.}$  air} centered on the space-time point  $(\vec{r}, t)$ . From dimensional analysis, note that

$$
\tilde{\rho}(\vec{r},t) \frac{D\vec{\tilde{u}}(\vec{r},t)}{Dt} \left(\frac{kg-m/s^2}{m^3} = \frac{N}{m^3}\right)
$$
 is a force density. The term  $\frac{D}{Dt} = \frac{\partial}{\partial t} + \vec{\tilde{u}}(\vec{r},t) \cdot \vec{\nabla}$  is known as

the *convective* (or *substantive* , *aka material*) derivative, computed from a *stationary* observer's reference frame, *e*.*g*. fixed in the *laboratory*:

$$
\frac{D}{Dt} = \frac{\partial}{\partial t} + \frac{\partial \tilde{x}(\vec{r},t)}{\partial t} \frac{\partial}{\partial x} + \frac{\partial \tilde{y}(\vec{r},t)}{\partial t} \frac{\partial}{\partial y} + \frac{\partial \tilde{z}(\vec{r},t)}{\partial t} \frac{\partial}{\partial z}
$$
\n
$$
= \frac{\partial}{\partial t} + \tilde{u}_x(\vec{r},t) \frac{\partial}{\partial x} + \tilde{u}_y(\vec{r},t) \frac{\partial}{\partial y} + \tilde{u}_z(\vec{r},t) \frac{\partial}{\partial z} = \frac{\partial}{\partial t} + (\tilde{\vec{u}}(\vec{r},t) \cdot \vec{\nabla})
$$

 Euler's equation for inviscid fluid flow is a first-order, linear, homogeneous differential equation, arising from consideration of momentum conservation in a *lossless***/***dissipationless* compressible fluid (liquid or gas), that in the absence of external driving forces describes the compression in Figure of gas), that in the absence of external driving forces describes the relationship between complex pressure  $\tilde{p}(\vec{r},t)$  and complex particle velocity  $\vec{\tilde{u}}(\vec{r},t)$  in the compressible fluid, of volume mass density  $\tilde{\rho}(\vec{r},t)$   $(kg/m^3)$ . Euler's equation for inviscid fluid flow is thus valid for fluids where the *viscosity* of the fluid and/or the *conduction* of *heat* in the fluid are *both* zero {or can both be *approximated* as being *negligible*}:

$$
\overline{\tilde{\rho}(\vec{r},t)\frac{D\vec{\tilde{u}}(\vec{r},t)}{Dt}} = \tilde{\rho}(\vec{r},t)\overline{\left(\frac{\partial\vec{\tilde{u}}(\vec{r},t)}{\partial t} + (\vec{\tilde{u}}(\vec{r},t)\cdot\vec{\nabla})\vec{\tilde{u}}(\vec{r},t)\right)} = -\vec{\nabla}\tilde{p}(\vec{r},t)
$$

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